



# THE STRUCTURAL CHANGES OF ASPHALTENES DURING HYDROCONVERSION

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# Introduction

## ASPHALTENES

Are the heaviest aromatic component of crude oil

Are precipitated on the catalyst surface and block the pore mouth

Act as coke precursors

May limit the maximum level of feedstock conversion

Catalyst deactivation

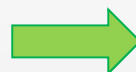
1. Investigation of the structure, composition and properties of macromolecular weight components
2. Study of their behavior and features of transformations during refining



Increase the efficiency of refining and control the process parameters and feedstock conversion

# Introduction

Hydroconversion in the presence of nanosized catalyst particles  $\text{MoS}_2$



Refining of different feedstock regardless of content:

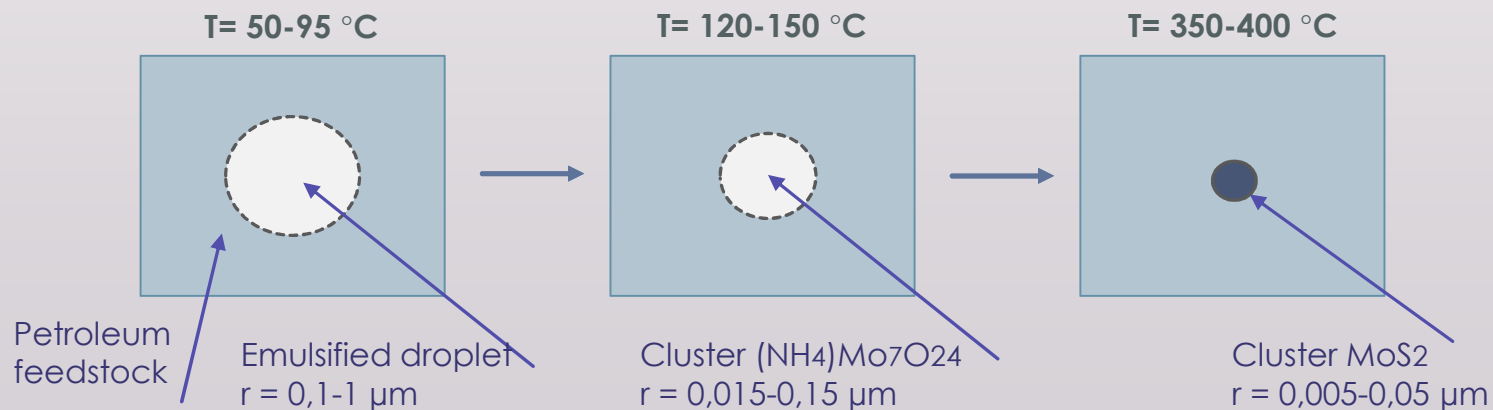
- heteroatoms;
- heavy metals;
- asphaltenes and resins.

Process provides:

- high conversion of feedstock;
- low coke formation;
- decrease in the pressure to 6-7 MPa.

**Catalyst precursors** – Water-soluble salts of catalytically active metals, that are introduced as emulsions followed by conversion to the slurry in heat treatment

Synthesis of nanosized catalyst particles  
“in situ” in the reaction zone:



# Experimental part

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## 1st experimental session:

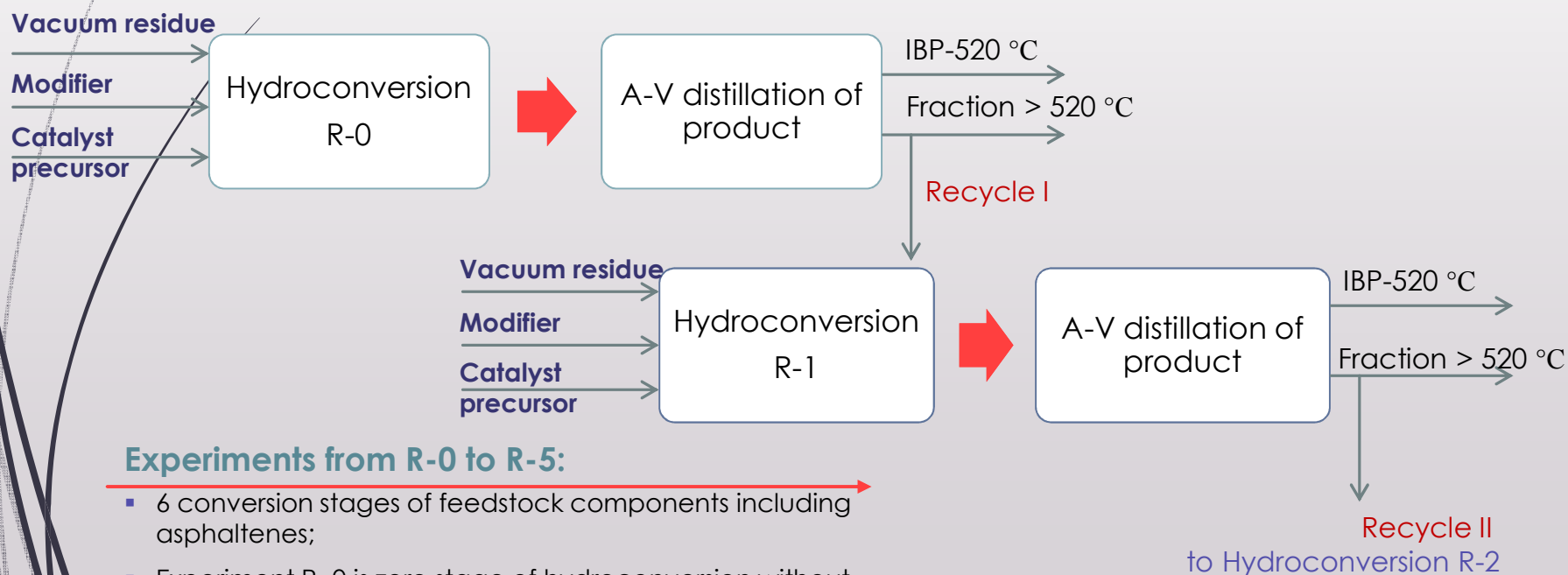
Various temperatures (425, 440, 445 и 450 °C)

- $T = 425\text{--}450^\circ\text{C}$ ,  $P = 7.0\text{ MPa}$ , liquid hourly space-velocity (LHSV) of  $2.0\text{--}2.2\text{ h}^{-1}$ , and hydrogen/feedstock ratio up to 1000 n L/L

## 2nd experimental session:

Various number of asphaltene conversion stages in the reaction zone

- $T = 440\text{--}445^\circ\text{C}$ ,  $P = 7.0\text{ MPa}$ , liquid hourly space-velocity (LHSV) of  $1.5\text{ h}^{-1}$ , and hydrogen/feedstock ratio up to 1000 n L/L



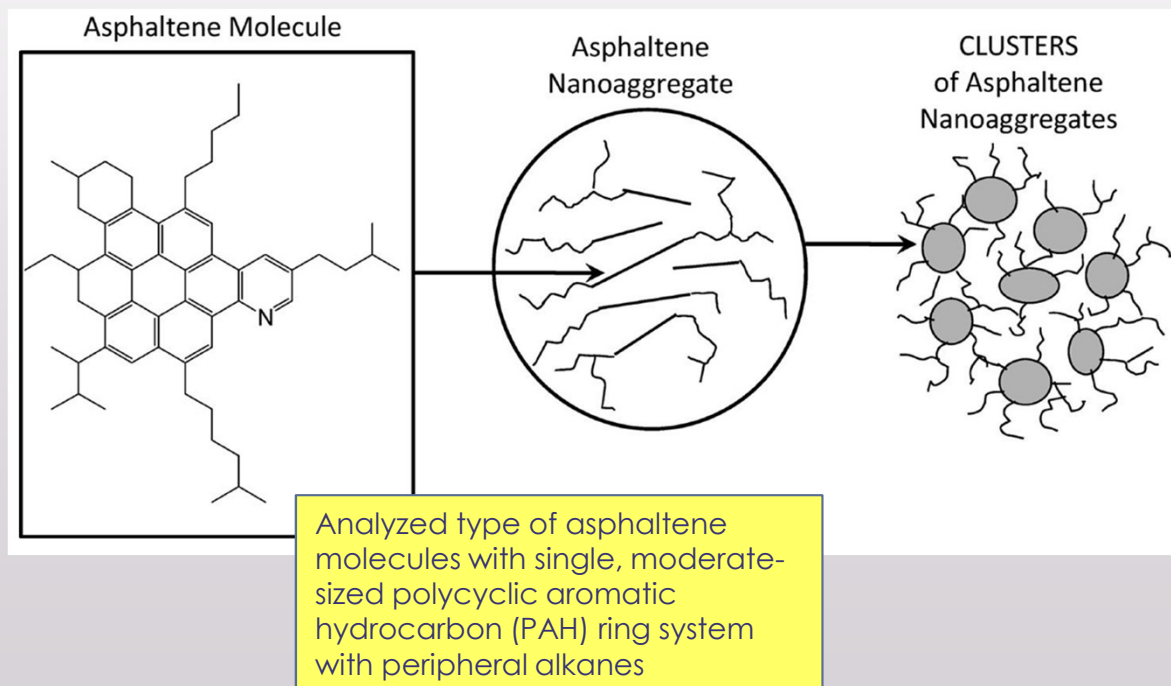
# Object of investigation

Asphaltenes from petroleum feedstock

Asphaltenes from hydroconversion products

Molecular structure

Colloidal structure



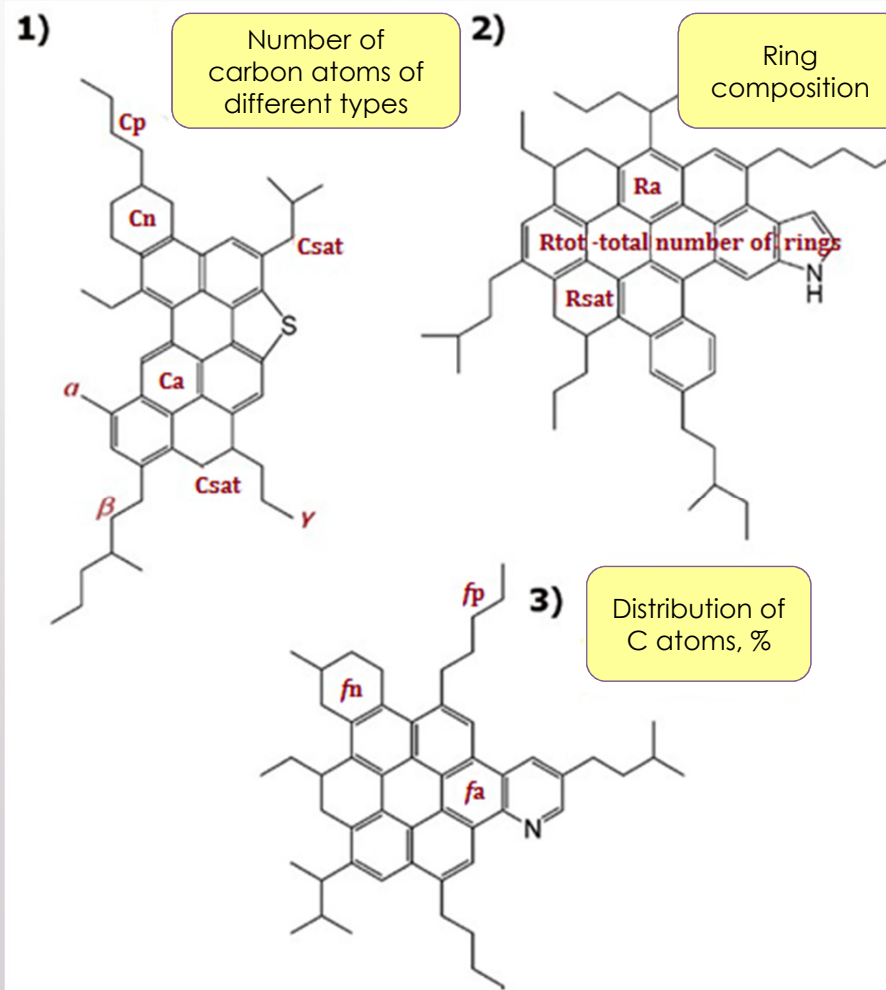
# The structural parameters of asphaltene molecules

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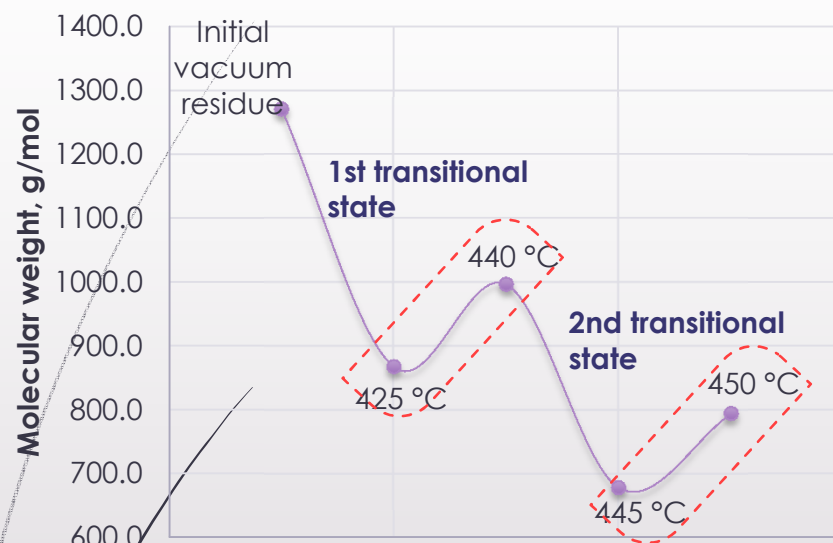
- Elemental composition;
- Average molecular weights;
- Distribution of hydrogen atoms;

Structural group analysis

Average distribution of carbon atoms between the structural elements



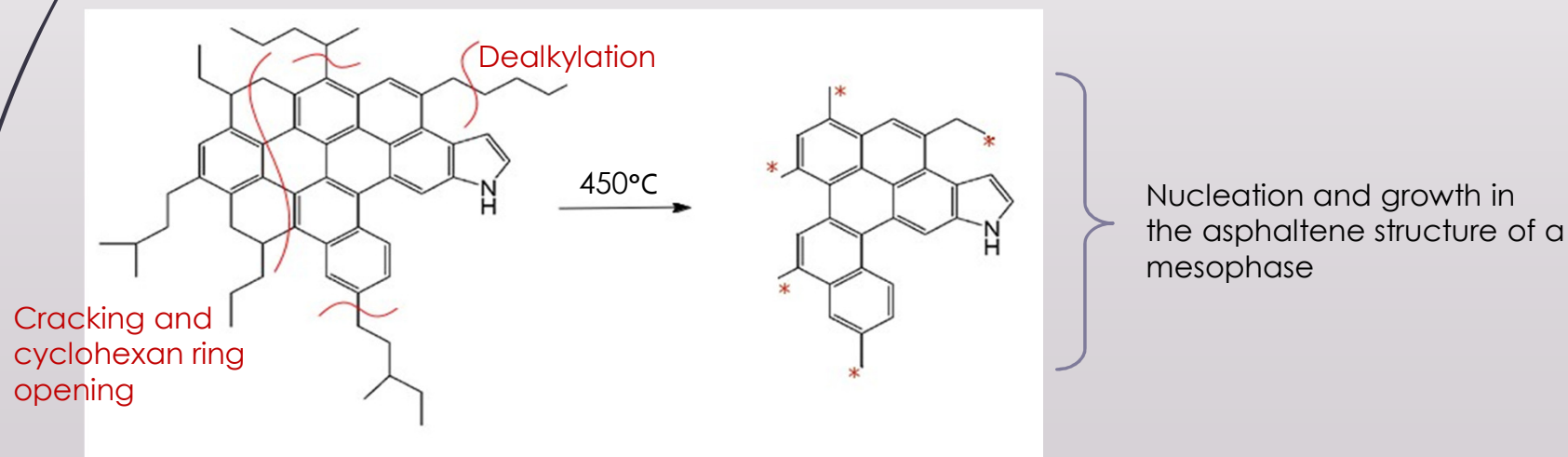
# Change in molecular weight of asphaltenes at various temperatures



One of the main features is the *nonmonotonic character* of changes in MW.

It has been noted:

- *Characteristic temperature ranges* – 425-440 °C and 445-450 °C;
- Low temperatures (below 425 °C) and the range 440-445 °C – *transitional states*.



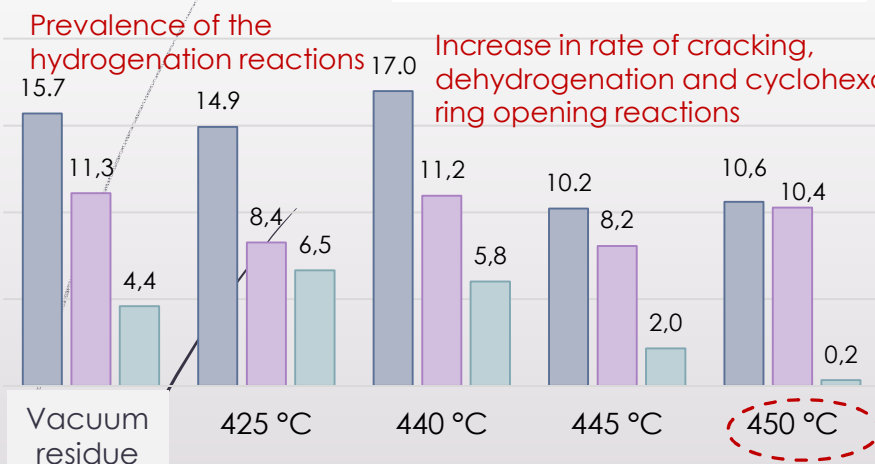
# Change in the ring composition (1), the amount of aromatic and saturated carbon atoms (2) in the structure of asphaltene molecules

1

- R<sub>tot</sub> – total number of rings
- R<sub>a</sub> – number of aromatic rings
- R<sub>sat</sub> – number of saturated rings

Prevalence of the hydrogenation reactions

Increase in rate of cracking, dehydrogenation and cyclohexane ring opening reactions

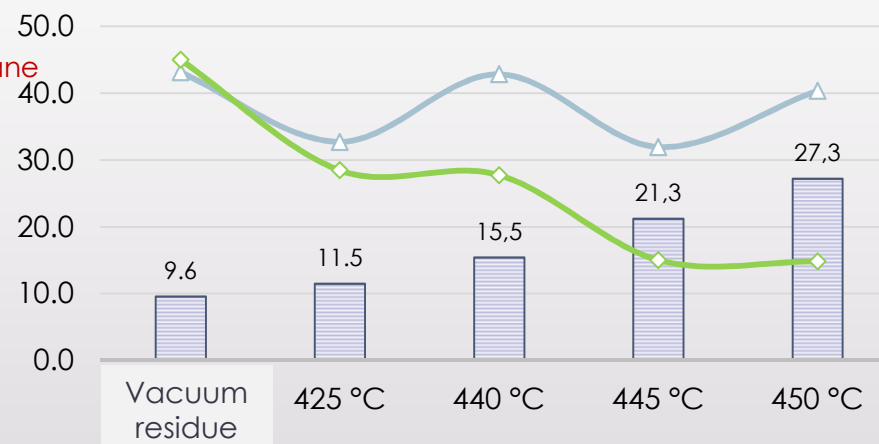


Stability of the size of the condensed aromatic core (R<sub>a</sub> ≈ const)

Increase in the proportion of unsubstituted aromatic rings (R<sub>a</sub>/R<sub>tot</sub> ≈ 1)

2

- (C<sub>a</sub>/C<sub>sat</sub>) × 10
- △— C<sub>a</sub> – number of aromatic carbon atoms
- ◇— C<sub>sat</sub> – number of saturated carbon atoms



Increase in the hydroconversion temperature →

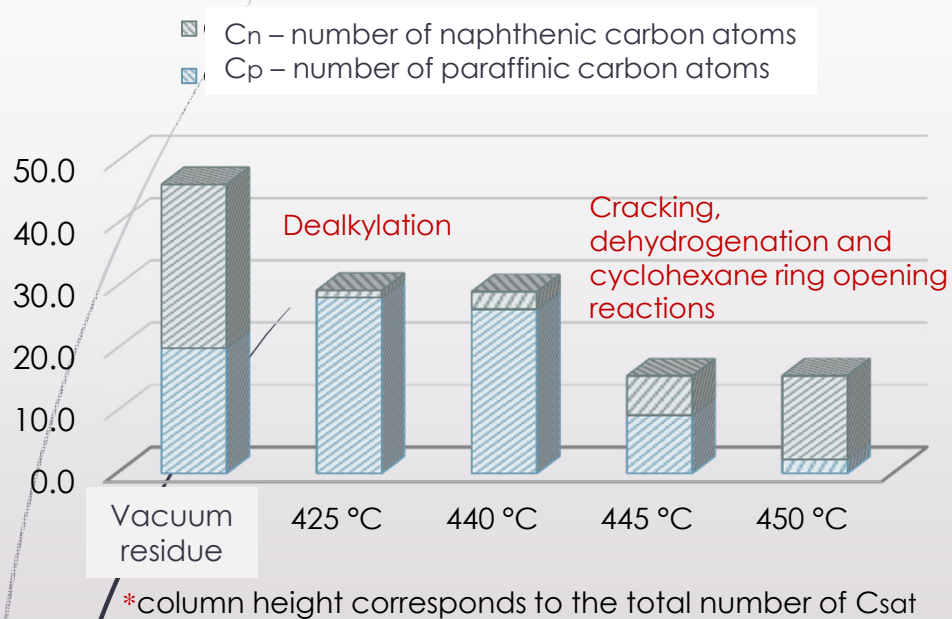
- Redistribution of carbon between aromatic and saturated fragments (C<sub>a</sub>/C<sub>sat</sub> > 1);
- Increase in aromaticity;
- Stability of the size of the condensed aromatic core (C<sub>a</sub> ≈ const)



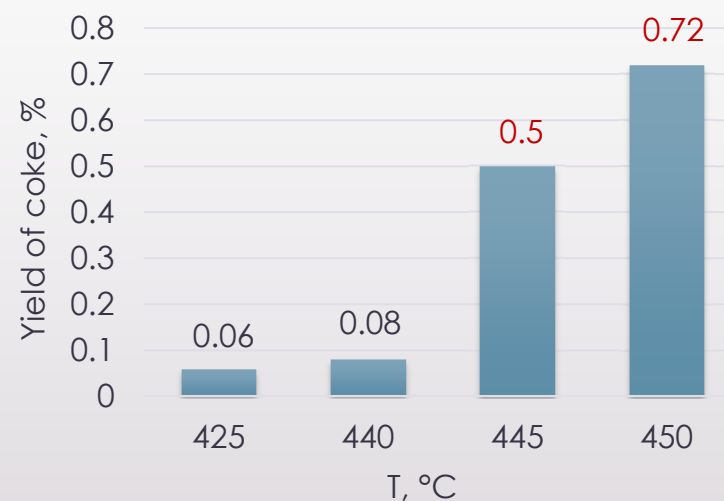
## Change in the amount of carbon atoms in naphthenic and paraffinic (1), influence of temperature on the yield of coke (2)

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1



2



Increase in the hydroconversion temperature to 440° C



Increase in the amount of unsubstituted aromatic rings



Nucleation and growth in the asphaltene phase of a mesophase



Significant increase in the amount of coke

# Scheme of structural transformations of asphaltene molecules depending on hydroconversion temperature

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Reduction in the amount saturated structures in the condensed naphthenic-aromatic core by considerable enhancement cracking and cyclohexan ring opening reactions; insignificant change in the amount of Ra

2<sup>nd</sup> TRANSITIONAL STATE

**Asphaltenes of hydroconversion products (425-440°C)**

Prevalence of saturated over aromatic structures  $Ca/C_{sat} < 1$

- a) Increase in aromaticity by the rise in the rate of dehydrogenation reactions of Rsat
- b) Low extent of suppression of hydrogenation reactions, stability of Rtot in the condensed naphthenic-aromatic core
- c) High degree of dealkylation

- a) Increase in the rate of dehydrogenation reactions, decrease in the degree of dealkylation
- b) Stability of Rtot
- c) Increase in the proportion of unsubstituted aromatic fragments

**Asphaltenes of vacuum residue**

**Asphaltenes of hydroconversion products (445-450°C)**

1<sup>st</sup> TRANSITIONAL STATE

- Prevalence of the hydrogenation reactions of aromatic fragments;
- High rate of dealkylation  $Ca/C_{sat} > 1$

**INCREASE IN THE HYDROCONVERSION TEMPERATURE**

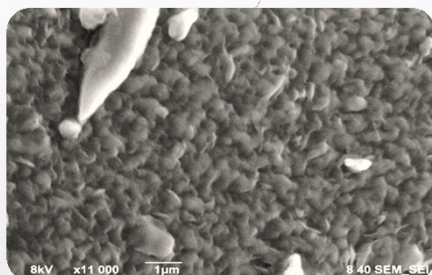
- ❑ Reduction in MW by the cracking, dealkylation and C-S, -N, -O bond opening reactions;
- ❑ Stability of the condensed aromatic core;
- ❑ Redistribution of carbon between aromatic and saturated fragments ( $Ca/C_{sat} > 1$ ); increase in the aromaticity.

# Change in asphaltene morphology depending on hydroconversion temperature

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SEM images

Asphaltenes from initial vacuum residue

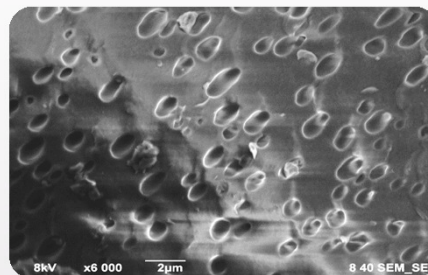


- Rough structure formed by the asphaltene aggregates, which are adsorbed on the surface of the resins.

1st transitional state

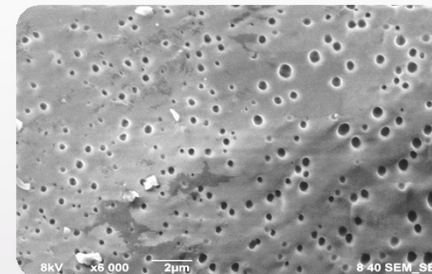


Asphaltenes from hydroconversion products at various temperatures



425°C

- Smooth surface with pores;
- Increasing temperature reduces pore size



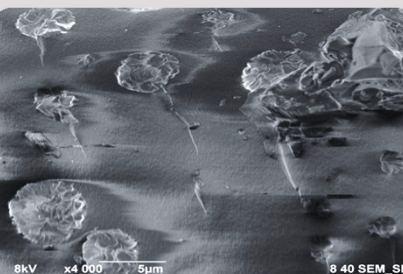
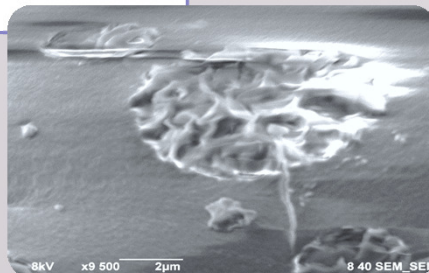
440°C

2nd transitional state

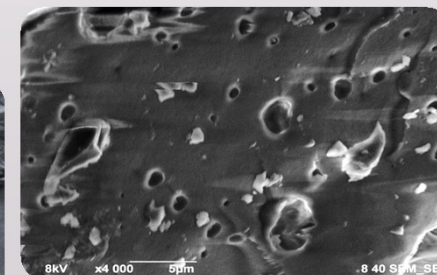


- Formation of stereospecific condensed structure in two-dimensional plane;
- Nucleation and growth in the asphaltene phase of a **mesophase**

Removal of alkyl chains and increase in the proportion of unsubstituted aromatic fragments



450°C



445°C

# Change in asphaltene morphology depending on hydroconversion temperature

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SEM images

The complex structural unit of resin-asphaltene constituents

The core (dispersed particles) is formed by paramagnetic asphaltene molecules

Adsorption-solvate layer composed of diamagnetic resin molecules and mono-, bi-, polycyclic aromatics

Spatial redistribution of macromolecular components and colloidal asphaltene structures

Aqueous solution of catalyst precursor

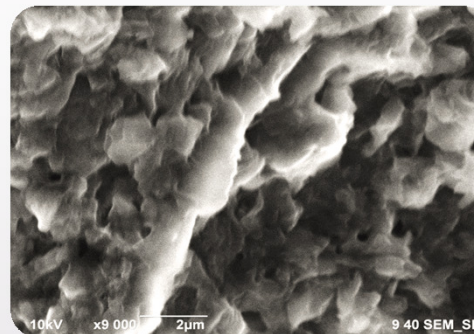
Structured interfacial layer (asphaltenes and resins)

Synthesis of catalytically active phase  $\text{MoS}_2$  "in situ" in the reaction zone

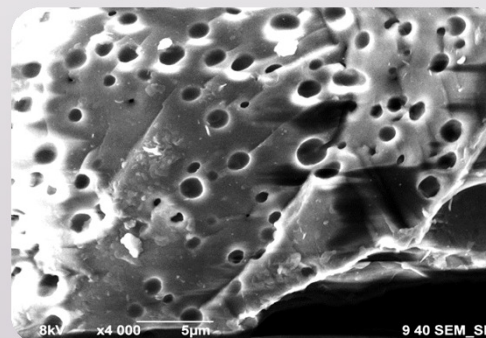
Additional dispergation of colloidal asphaltene structures, resins desorption

Increase in efficiency of contact between reactive molecules, catalyst and hydrogen

Emulsion – vacuum residue/ aqueous solution of catalyst precursor

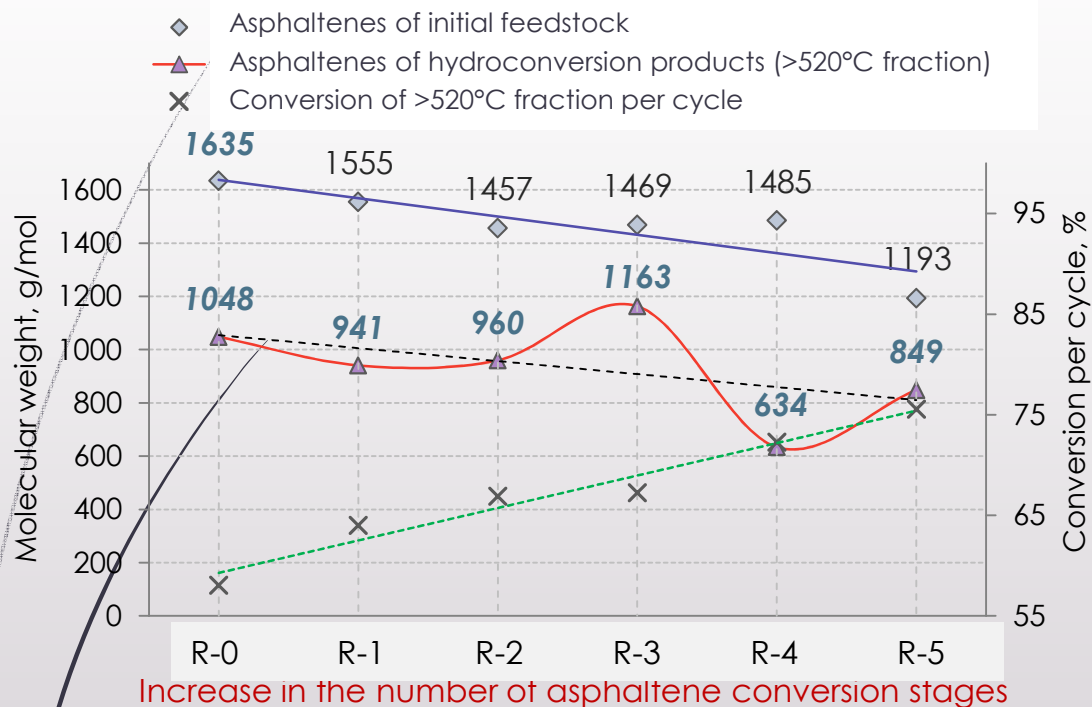


Slurry – vacuum residue/ nanosized catalyst particles  $\text{MoS}_2$



# Change in molecular weight depending on the number of asphaltene conversion stages

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Increase in the feedstock conversion per cycle

Decrease in MW of asphaltenes from processing products compared to MW of 1635 g/mol for initial feedstock asphaltenes

Asphaltenes from vacuum residue

**1st transitional state**

Zero stage of hydroconversion (R-0)

Asphaltenes from hydroconversion products

**2nd transitional state**

On the boundary between R-3 and R-4

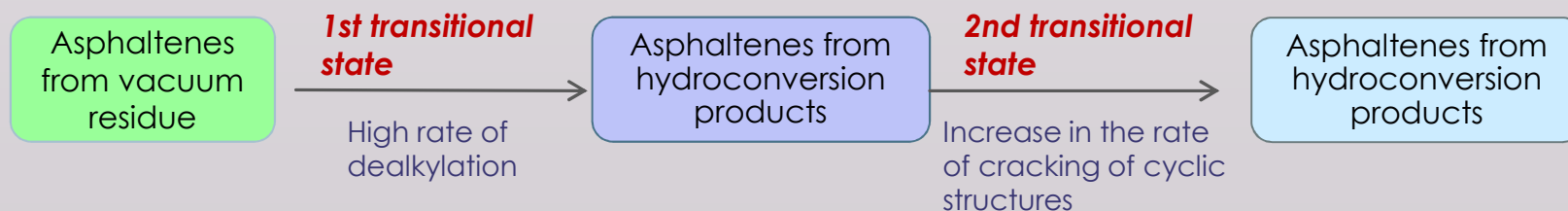
Asphaltenes from hydroconversion products



# Average structural parameters for asphaltene molecules

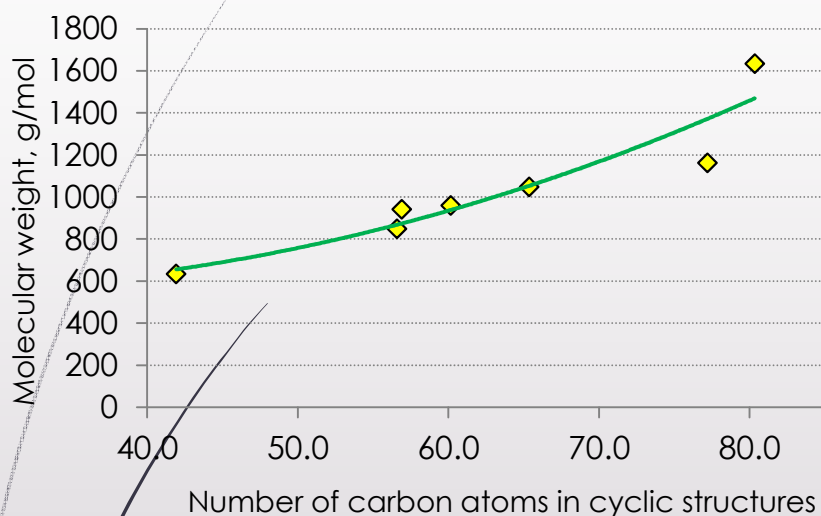
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Parameter	Asphaltenes of initial feedstock	Asphaltenes of hydroconversion product at different numbers of conversion stages					
		R-0	R-1	R-2	R-3	R-4	R-5
Average number of atoms in molecule							
C	110.2	73.2	65.1	67.7	82.7	43.6	58.7
H	118.2	61.7	58.0	56.4	70.0	38.5	50.3
N	2.0	1.7	1.4	1.6	2.0	0.8	1.2
S	3.7	1.8	1.8	1.7	2.2	0.8	1.2
O	2.9	1.5	1.5	0.8	0.1	2.2	2.4
Ring composition							
Ra	16.3	13.8	11.6	13.1	15.3	7.3	10.2
Rsat	4.6	2.8	2.9	2.2	4.3	3.2	4.0
Rtot	20.9	16.6	14.5	15.3	19.6	10.5	14.2
Average number of carbon atoms of different types in molecule							
Ca	61.4	53.4	45.0	50.9	59.2	28.7	39.6
Csat	48.8	19.8	20.1	16.8	23.5	14.9	19.1
Cc	80.3	65.4	56.9	60.2	77.2	41.9	56.6
Cn	18.9	12.0	11.9	9.3	18.0	13.2	17.0
Cp	29.9	7.8	8.2	7.5	5.5	1.7	2.1



Correlation of MW with the proportion of C atoms in the cyclic structures (1), change in the amount of heteroatoms depending on the amount of aromatic C atoms (2)

1)



As the number of asphaltene conversion stages increases, the amount of the most reactive compounds of sulfur decreases

Level of denitrogenation is less than desulfurization

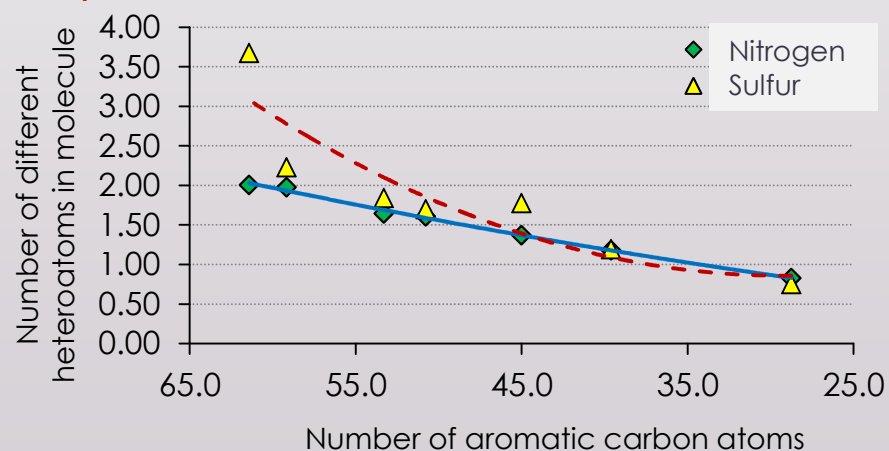
Stability of the condensed aromatic core ( $Ra \approx \text{const}$ )

Variation of temperature

Change in the number of recycling stages

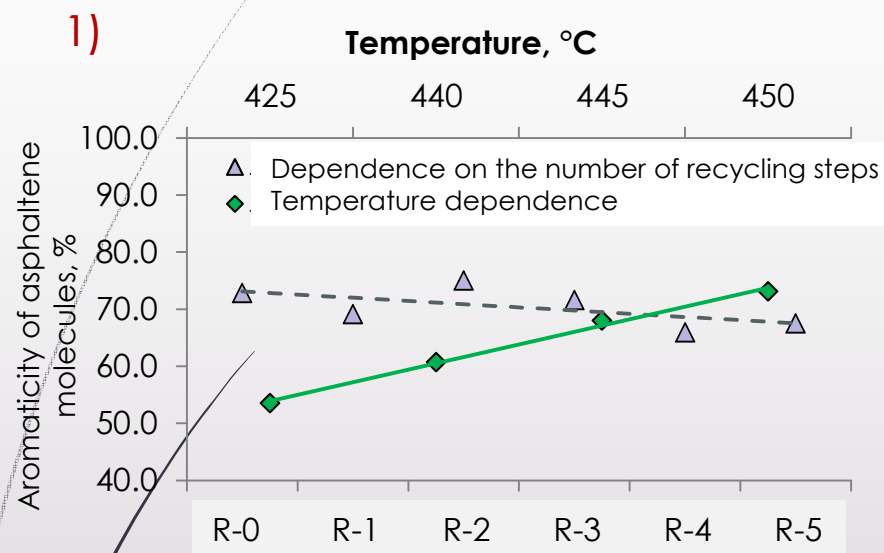
Destruction of cyclic fragments including the most stable heteroaromatic structures having low reactivity, with the high reaction rate of dealkylation

2)



Increase in the number of asphaltene conversion stages

## Dependence of the aromaticity (1) and the yield of condensation products (2) on the temperature and the number of conversion stages



Even and continuous growth of aromaticity molecules

↑ Increase in the hydroconversion temperature

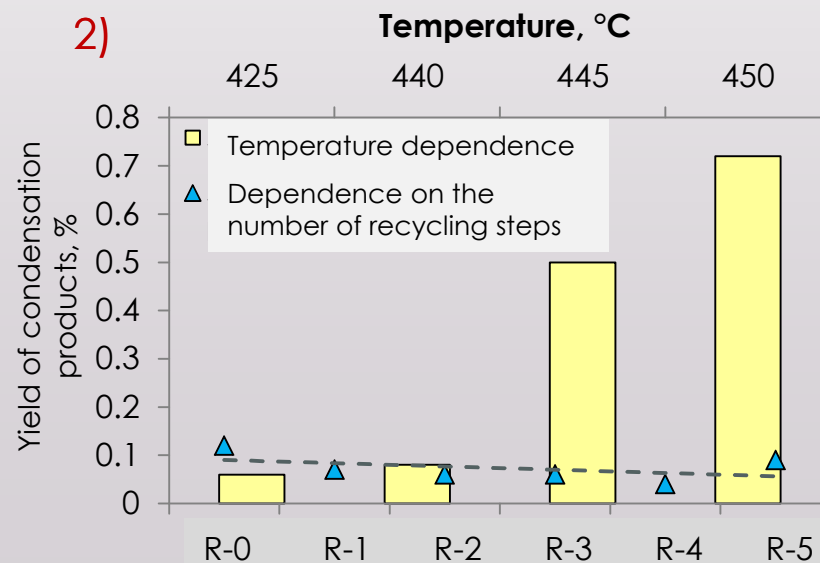
↓ Increase in the number of recycling stages

Decrease in aromaticity molecules

Increase in the hydroconversion temperature to 440° C

Increase in the amount of unsubstituted aromatic rings

Significant increase in the amount of coke





# Conclusion

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- It is shown that, the molecular structure of asphaltenes depending on different process conditions vary in a discrete manner, passing through a step of *transitional state* (TS), in which system is the most susceptible to the action of external factor.
- It is noted that, the changes in the structural parameters of asphaltene molecules at each TS step are due to the prevalence of characteristic reactions, which are similar as in variation of temperature and change in the number of recycling stages. However, there are significant differences between structural transformations of asphaltenes depending on various process parameters.
- Investigations of changes in asphaltene morphology confirm the main features of the structural transformations of asphaltenes, which were established by structural-group analysis of asphaltene molecules. It is shown that the quality rearrangement of the asphaltene molecular structure by passing through the TS, where the system is most active, leads to quality changes in the asphaltene morphology and change of colloidal-chemical structure of the system.
- Hydroconversion parameter intervals, corresponding to the TS, are the most favorable in terms of regulation of structural transformations of macromolecular components and increasing level of conversion with low coke formation.



**Thank you for attention!**