



THE STRUCTURAL CHANGES OF ASPHALTENES DURING HYDROCONVERSION

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Introduction

ASPHALTENES

Are the heaviest aromatic component of crude oil

Are precipitated on the catalyst surface and block the pore mouth

Act as coke precursors

May limit the maximum level of feedstock conversion

Catalyst deactivation

1. Investigation of the structure, composition and properties of macromolecular weight components
2. Study of their behavior and features of transformations during refining

Increase the efficiency of refining and control the process parameters and feedstock conversion

Introduction

Hydroconversion in the presence of nanosized catalyst particles MoS_2

Refining of different feedstock regardless of content:

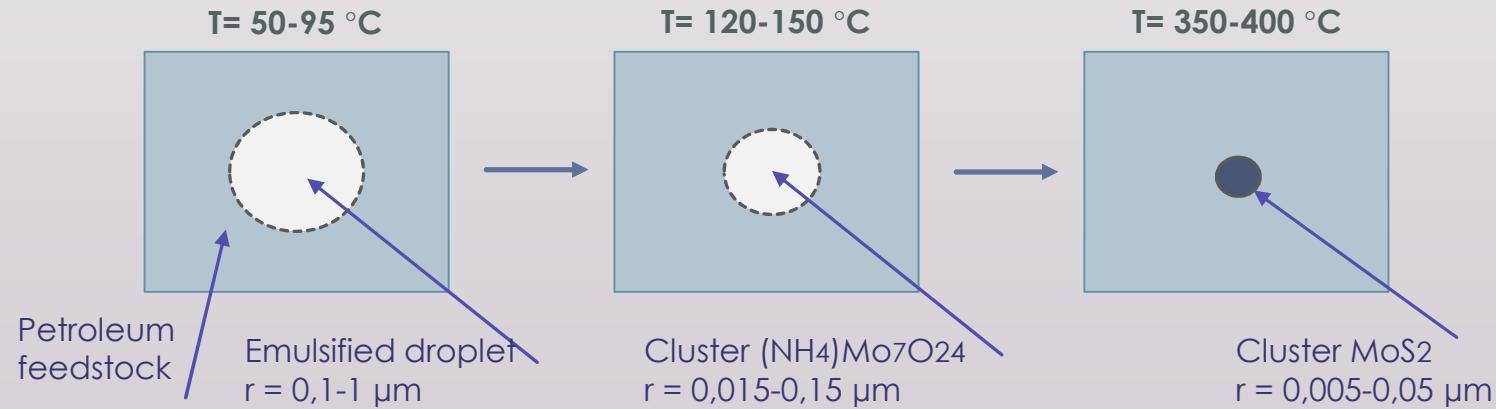
- heteroatoms;
- heavy metals;
- asphaltenes and resins.

Process provides:

- high conversion of feedstock;
- low coke formation;
- decrease in the pressure to 6-7 MPa.

Catalyst precursors – Water-soluble salts of catalytically active metals, that are introduced as emulsions followed by conversion to the slurry in heat treatment

Synthesis of nanosized catalyst particles
“in situ” in the reaction zone:



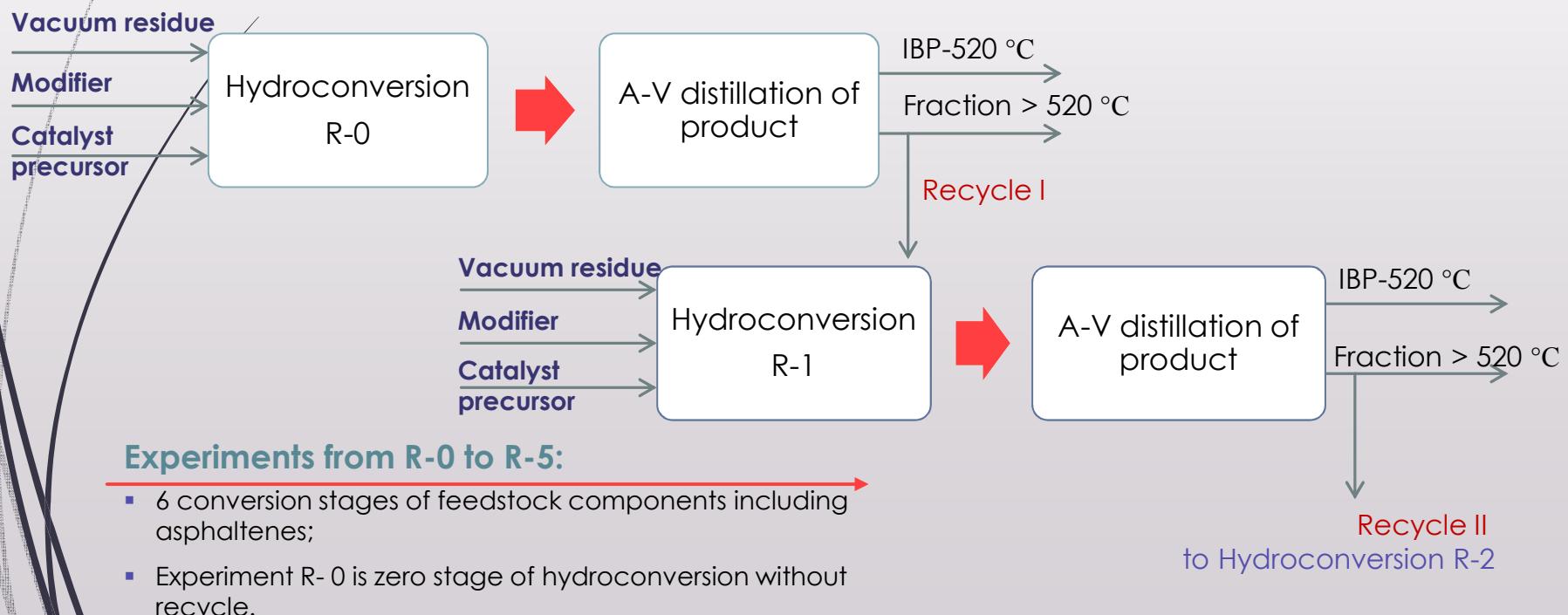
Experimental part

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1st experimental session:

Various temperatures (425, 440, 445 и 450 °C)

- $T = 425\text{--}450^\circ\text{C}$, $P = 7.0 \text{ MPa}$, liquid hourly space-velocity (LHSV) of $2.0\text{--}2.2 \text{ h}^{-1}$, and hydrogen/feedstock ratio up to 1000 n L/L



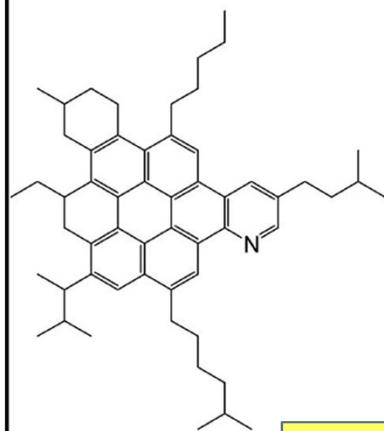
Object of investigation

Asphaltenes from petroleum feedstock

Asphaltenes from hydroconversion products

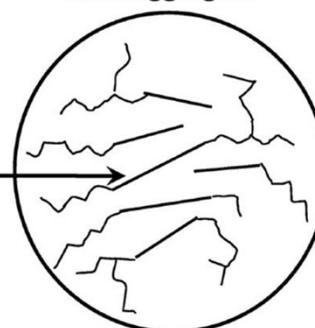
Molecular structure

Asphaltene Molecule

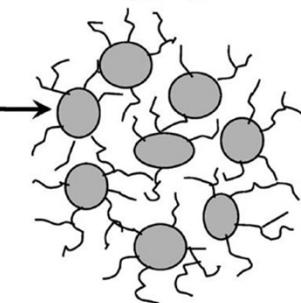


Colloidal structure

Asphaltene Nanoaggregate



CLUSTERS
of Asphaltene
Nanoaggregates



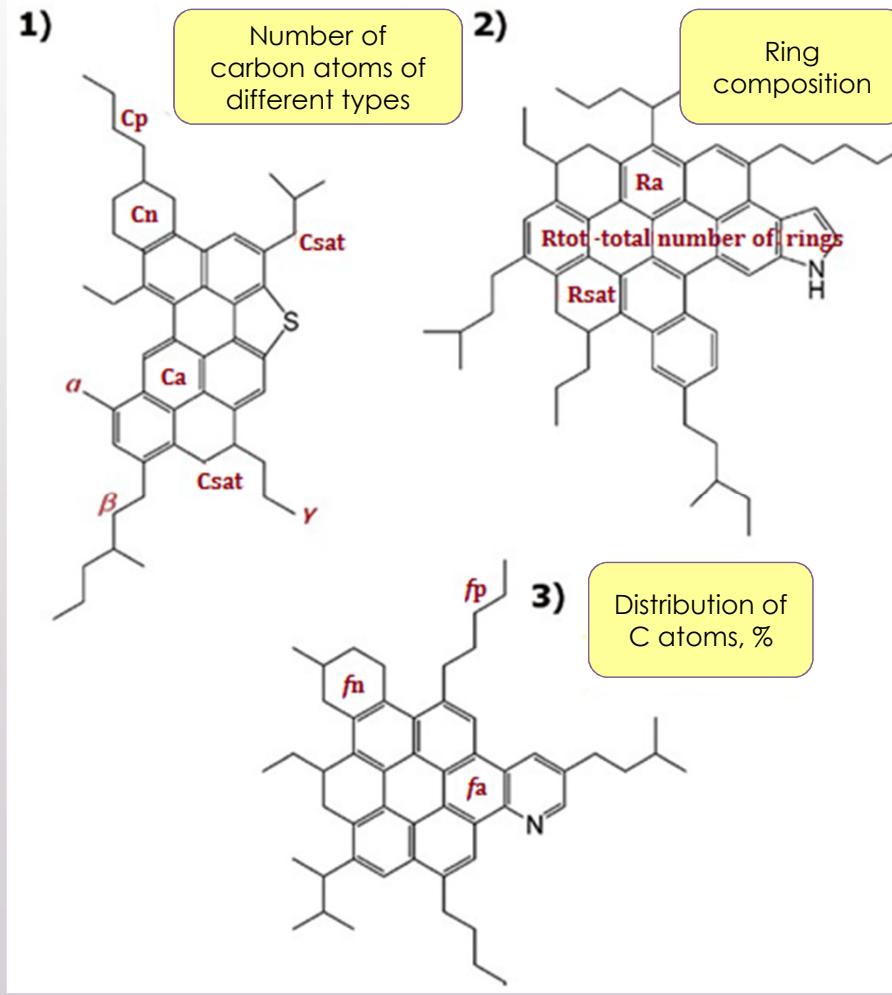
Analyzed type of asphaltene molecules with single, moderate-sized polycyclic aromatic hydrocarbon (PAH) ring system with peripheral alkanes

The structural parameters of asphaltene molecules

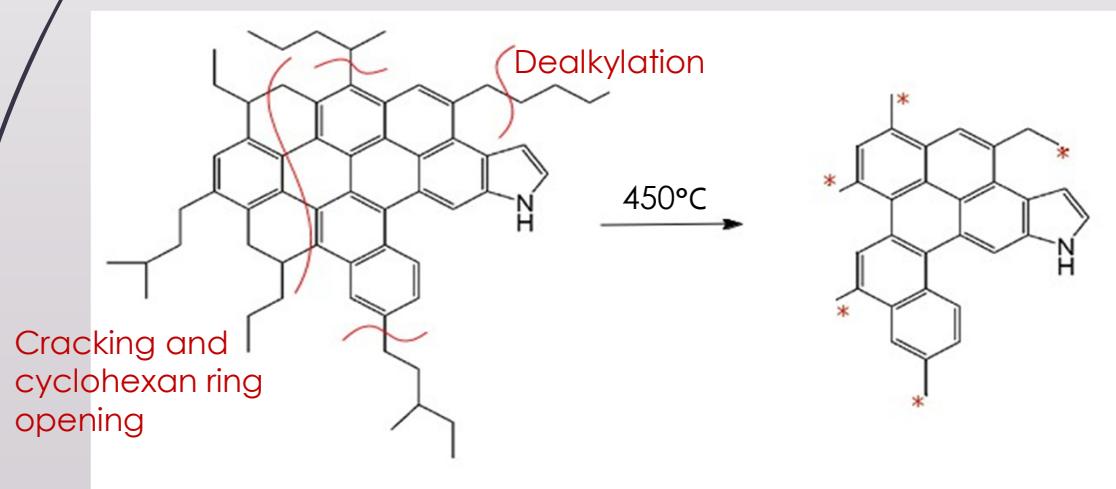
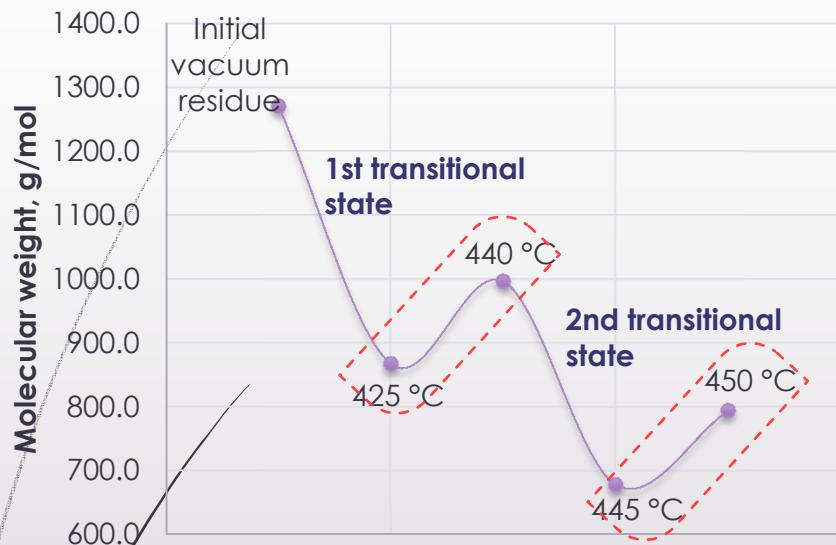
- Elemental composition;
- Average molecular weights;
- Distribution of hydrogen atoms;

Structural group analysis

Average distribution of carbon atoms between the structural elements



Change in molecular weight of asphaltenes at various temperatures



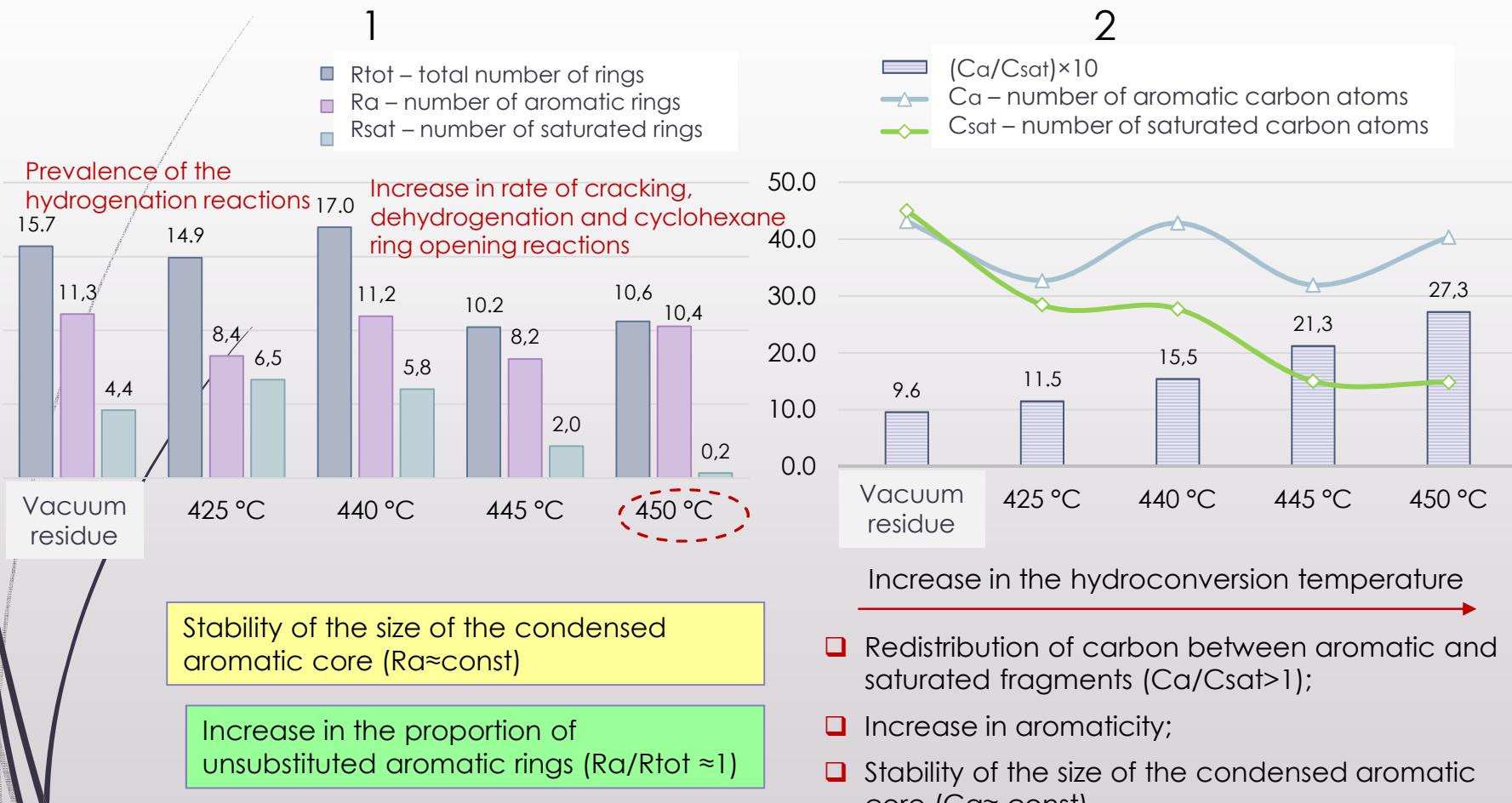
One of the main features is the **nonmonotonic character** of changes in MW.

It has been noted:

- **Characteristic temperature ranges** – 425-440 °C and 445-450 °C;
- Low temperatures (below 425 °C) and the range 440-445 °C – **transitional states**.

Nucleation and growth in the asphaltene structure of a mesophase

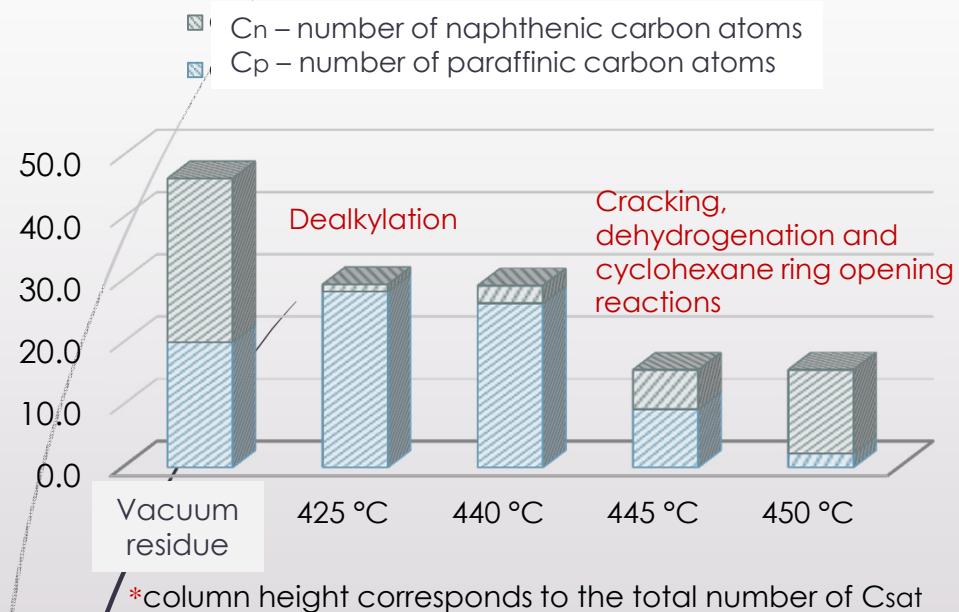
Change in the ring composition (1), the amount of aromatic and saturated carbon atoms (2) in the structure of asphaltene molecules



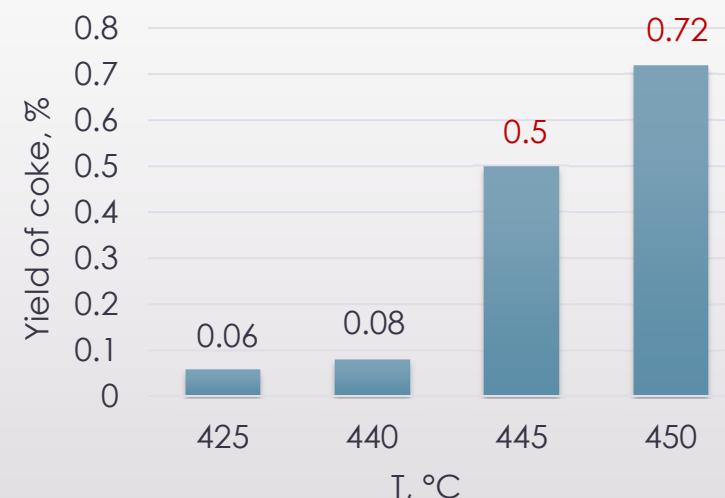
Change in the amount of carbon atoms in naphthenic and paraffinic (1), influence of temperature on the yield of coke (2)

9

1



2



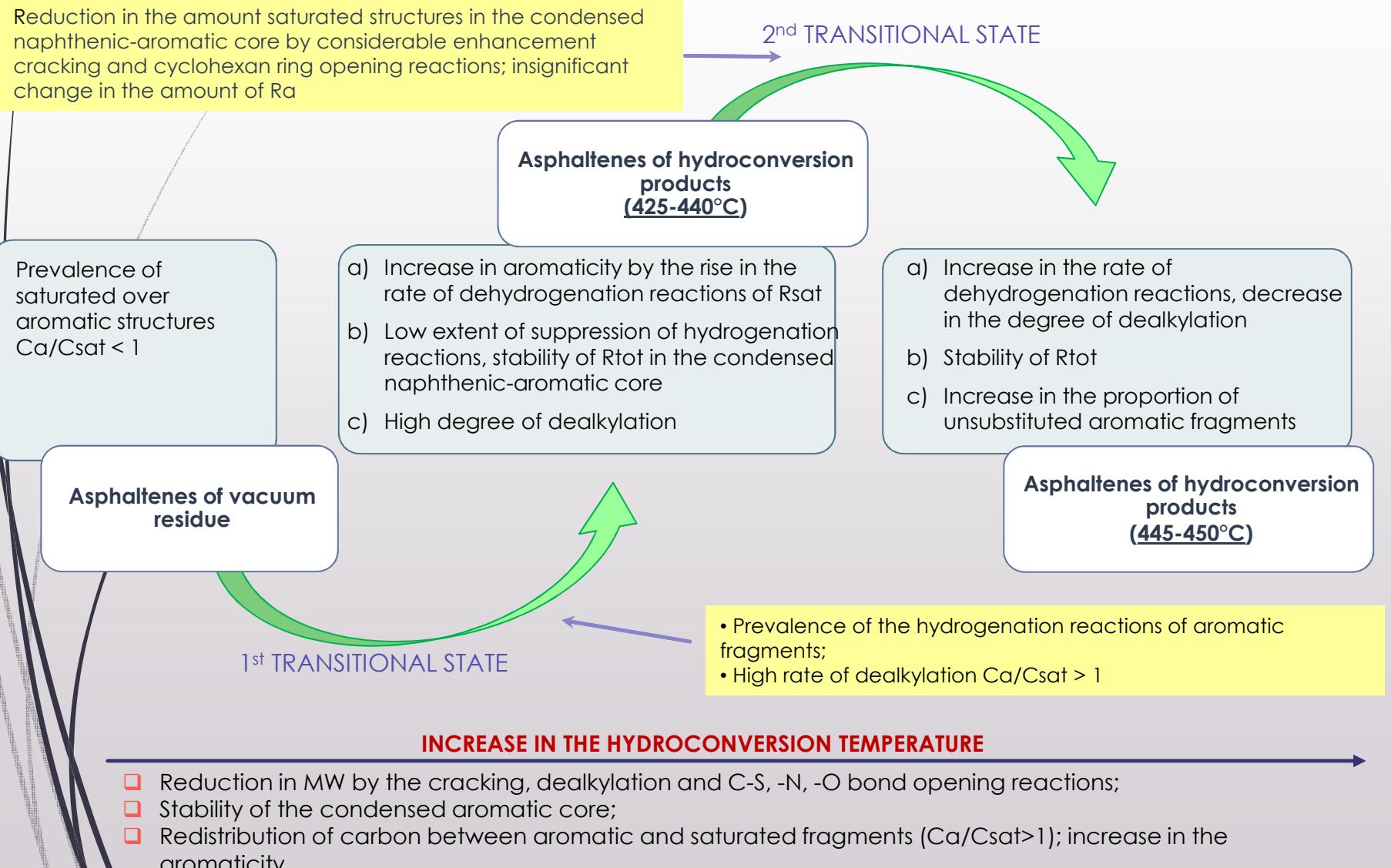
Increase in the hydroconversion temperature to 440° C

Increase in the amount of unsubstituted aromatic rings

Nucleation and growth in the asphaltene phase of a mesophase

Significant increase in the amount of coke

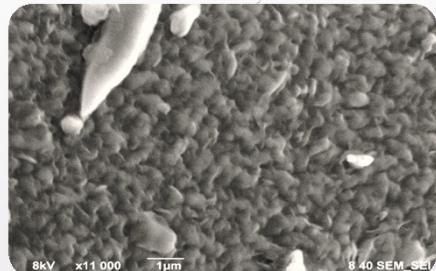
Scheme of structural transformations of asphaltene molecules depending on hydroconversion temperature



Change in asphaltene morphology depending on hydroconversion temperature

SEM images

Asphaltenes from initial vacuum residue



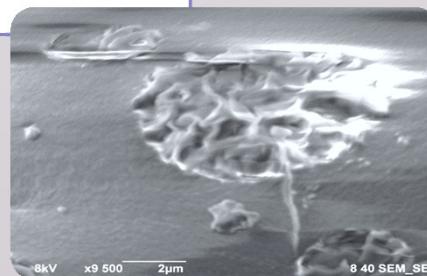
1st transitional state

- Rough structure formed by the asphaltene aggregates, which are adsorbed on the surface of the resins.

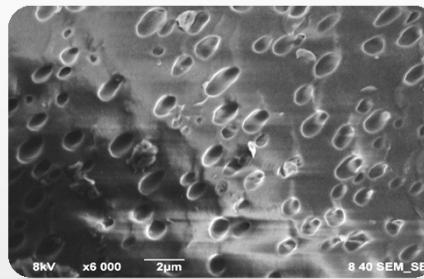


Removal of alkyl chains and increase in the proportion of unsubstituted aromatic fragments

- Formation of stereospecific condensed structure in two-dimensional plane;
- Nucleation and growth in the asphaltene phase of a **mesophase**

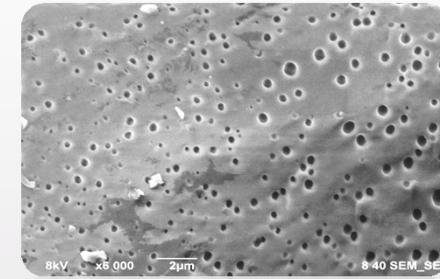


Asphaltenes from hydroconversion products at various temperatures



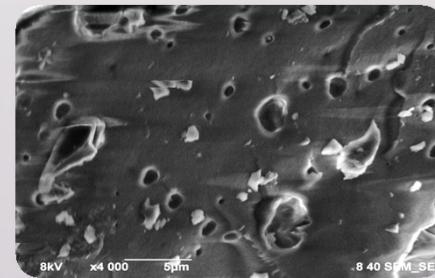
425°C

- Smooth surface with pores;
- Increasing temperature reduces pore size



440°C

2nd transitional state



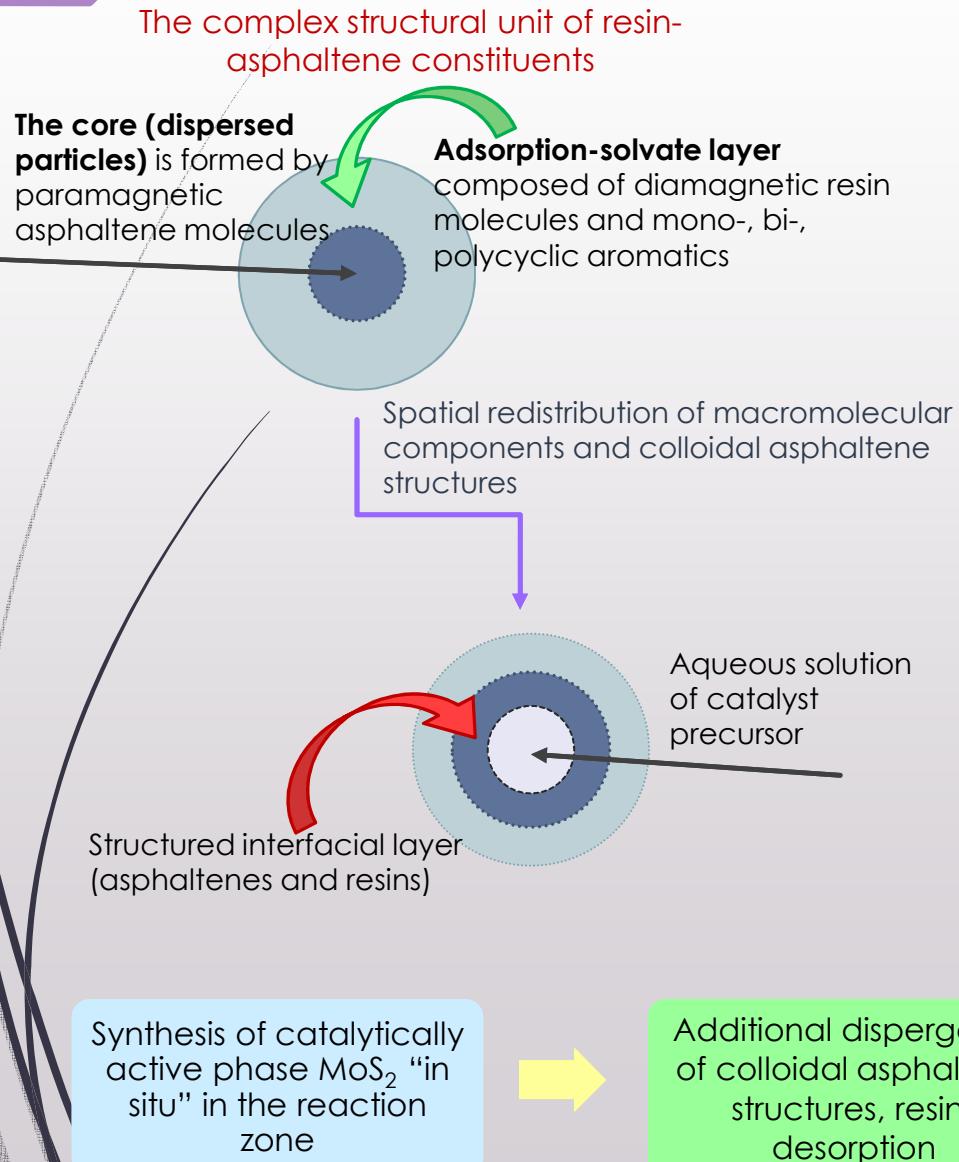
445°C

450°C

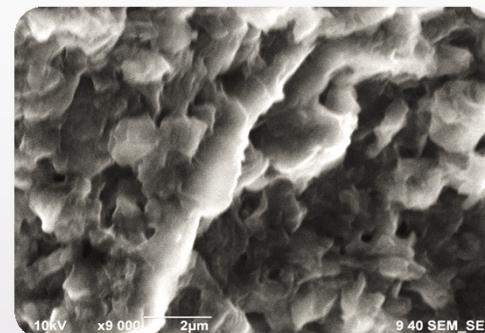
Change in asphaltene morphology depending on hydroconversion temperature

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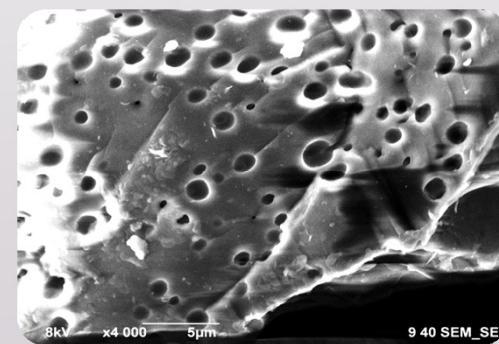
SEM images



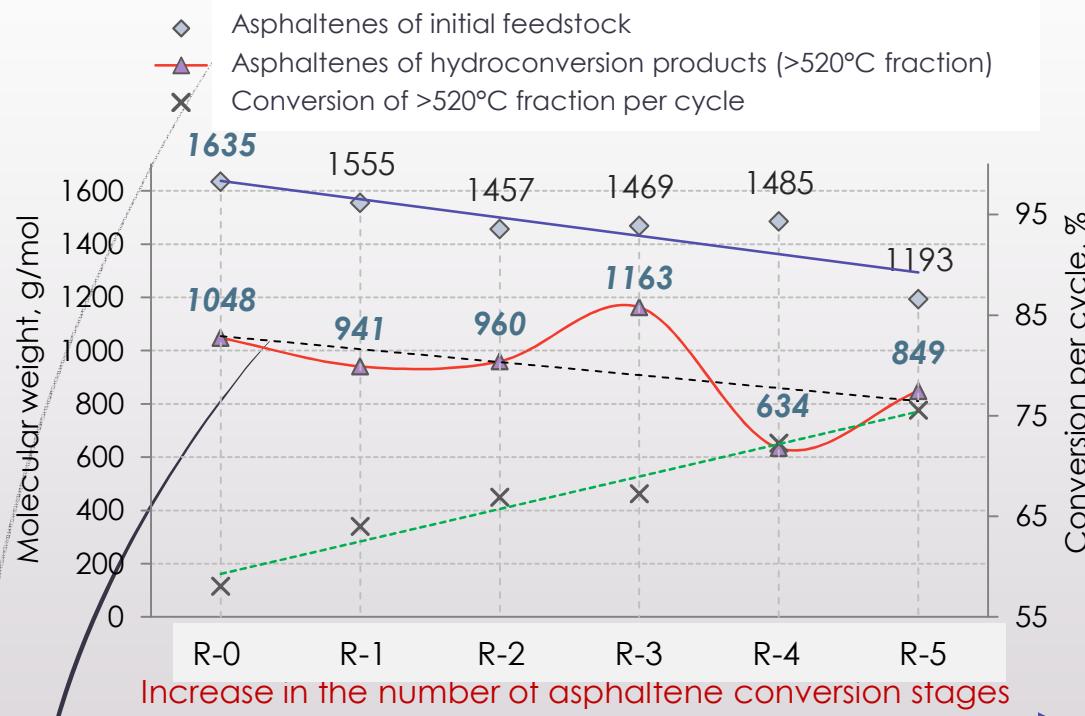
Emulsion – vacuum residue/ aqueous solution of catalyst precursor



Slurry – vacuum residue/ nanosized catalyst particles MoS_2



Change in molecular weight depending on the number of asphaltene conversion stages



Increase in the feedstock conversion per cycle

Decrease in MW of asphaltenes from processing products compared to MW of 1635 g/mol for initial feedstock asphaltenes

Nonmonotonic character of changes in MW

Asphaltenes from vacuum residue

1st transitional state

Zero stage of hydroconversion (R-0)

Asphaltenes from hydroconversion products

2nd transitional state

On the boundary between R-3 and R-4

Asphaltenes from hydroconversion products

Average structural parameters for asphaltene molecules

Parameter	Asphaltenes of initial feedstock	Asphaltenes of hydroconversion product at different numbers of conversion stages					
		R-0	R-1	R-2	R-3	R-4	R-5
Average number of atoms in molecule							
C	110.2	73.2	65.1	67.7	82.7	43.6	58.7
H	118.2	61.7	58.0	56.4	70.0	38.5	50.3
N	2.0	1.7	1.4	1.6	2.0	0.8	1.2
S	3.7	1.8	1.8	1.7	2.2	0.8	1.2
O	2.9	1.5	1.5	0.8	0.1	2.2	2.4
Ring composition							
R _a	16.3	13.8	11.6	13.1	15.3	7.3	10.2
R _{sat}	4.6	2.8	2.9	2.2	4.3	3.2	4.0
R _{tot}	20.9	16.6	14.5	15.3	19.6	10.5	14.2
Average number of carbon atoms of different types in molecule							
C _a	61.4	53.4	45.0	50.9	59.2	28.7	39.6
C _{sat}	48.8	19.8	20.1	16.8	23.5	14.9	19.1
C _c	80.3	65.4	56.9	60.2	77.2	41.9	56.6
C _n	18.9	12.0	11.9	9.3	18.0	13.2	17.0
C _p	29.9	7.8	8.2	7.5	5.5	1.7	2.1

Asphaltenes from vacuum residue

1st transitional state

High rate of dealkylation

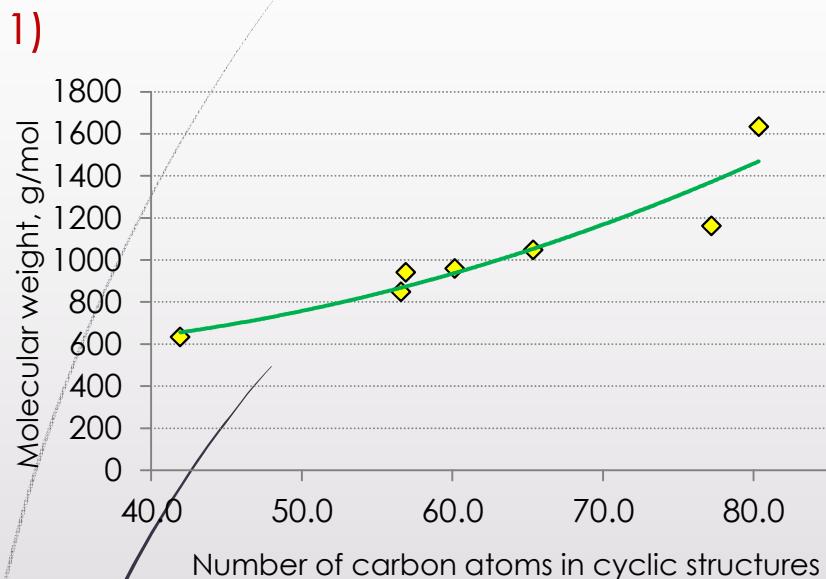
Asphaltenes from hydroconversion products

2nd transitional state

Increase in the rate of cracking of cyclic structures

Asphaltenes from hydroconversion products

Correlation of MW with the proportion of C atoms in the cyclic structures (1), change in the amount of heteroatoms depending on the amount of aromatic C atoms (2)



As the number of asphaltene conversion stages increases, the amount of the most reactive compounds of sulfur decreases

Level of denitrogenation is less than desulfurization

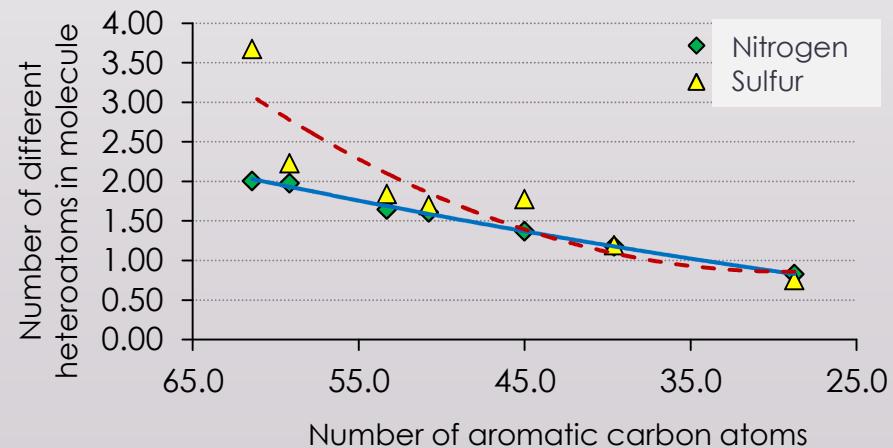
Stability of the condensed aromatic core
($R_a \approx \text{const}$)

Variation of temperature

Change in the number of recycling stages

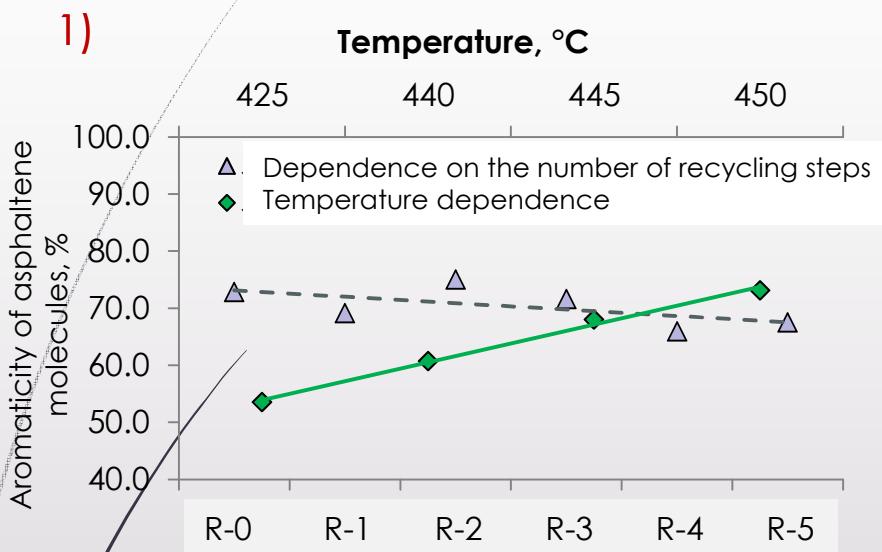
Destruction of cyclic fragments including the most stable heteroaromatic structures having low reactivity, with the high reaction rate of dealkylation

2)



Increase in the number of asphaltene conversion stages

Dependence of the aromaticity (1) and the yield of condensation products (2) on the temperature and the number of conversion stages



Increase in the hydroconversion temperature to 440°C

Increase in the amount of unsubstituted aromatic rings

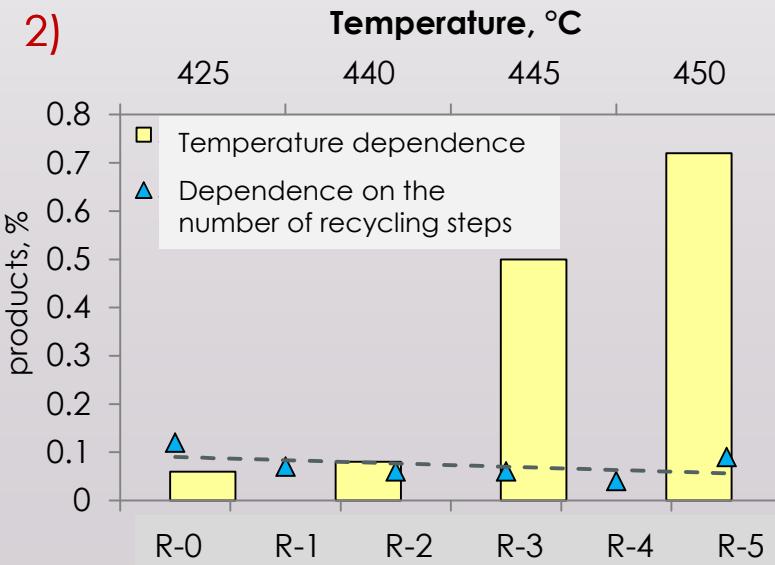
Significant increase in the amount of coke

Even and continuous growth of aromaticity molecules

↑ Increase in the hydroconversion temperature

↓ Increase in the number of recycling stages

Decrease in aromaticity molecules



Conclusion

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- It is shown that, the molecular structure of asphaltenes depending on different process conditions vary in a discrete manner, passing through a step of *transitional state* (TS), in which system is the most susceptible to the action of external factor.
- It is noted that, the changes in the structural parameters of asphaltene molecules at each TS step are due to the prevalence of characteristic reactions, which are similar as in variation of temperature and change in the number of recycling stages. However, there are significant differences between structural transformations of asphaltenes depending on various process parameters.
- Investigations of changes in asphaltene morphology confirm the main features of the structural transformations of asphaltenes, which were established by structural-group analysis of asphaltene molecules. It is shown that the quality rearrangement of the asphaltene molecular structure by passing through the TS, where the system is most active, leads to quality changes in the asphaltene morphology and change of colloidal-chemical structure of the system.
- Hydroconversion parameter intervals, corresponding to the TS, are the most favorable in terms of regulation of structural transformations of macromolecular components and increasing level of conversion with low coke formation.



Thank you for attention!